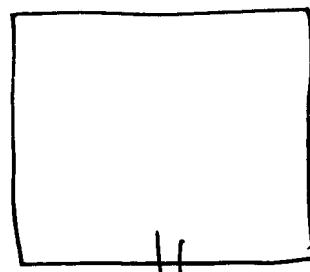


Problem 5.36

What is the final temp. (T_2),
Work ($\pm W_2$) and heat transfer
($\pm Q_2$) ?



$$P_1 = 1200 \text{ kPa}$$

$$T_1 = 300^\circ \text{C}$$

Container
 $m = 0.75 \text{ kg}$
(water)

Cooling
(Final temperature $P_2 = 300 \text{ kPa}$)

Solution: Fix state 1

1. Sat. Table (B.1.2; Page 680)

$$\text{for } P_1 = 1200 \text{ kPa} \Rightarrow T_{\text{sat}} = 187.99^\circ \text{C}$$

2. Since $T_1 > T_{\text{sat}} \Rightarrow$ State is superheated.

At 1200 kPa, 300°C (Table B.1.3; page 684)

$$v_1 = 0.21382 \text{ m}^3/\text{kg}$$

$$u_1 = 2789.22 \text{ kJ/kg}$$

Process is constant volume ($v=c$): $v_2 = v_1$

(Since $v_2 = v_1$; and $m_2 = m_1$).

In final state 2, $v_2 = 0.21382 \text{ m}^3/\text{kg}$

$$P_2 = 300 \text{ kPa.}$$

Fix. state 2: Sat. Table (B.1.2; Page 678)

$$\text{at } P_2 = 300 \text{ kPa} \Rightarrow v_f = 0.001073 \text{ m}^3/\text{kg}$$

$$v_g = 0.60582 \text{ m}^3/\text{kg}$$

Since $v_f \leq v_2 \leq v_g \Rightarrow$ state 2 is saturated.

- Calculate quality x_2

$$u_2 = v_f + x_2 v_{fg} \Rightarrow x_2 = (u_2 - v_f) / v_{fg}$$

$$x_2 = (0.21382 - 0.001073) / 0.60475$$

$$x_2 = 0.351$$

- $u_2 = u_f + x_2 u_{fg} = 561.13 + 0.351 * 1982.43$

$$u_2 = 1258.5355$$

$$m_2 = m_1 = \frac{V}{v} \quad m = 0.75 \text{ kg.}$$

- Work $\Delta W_2 = 0$ Since constant volume process is carried out.

$$\Delta W_2 = \int_{V_1}^{V_2} P dV = 0 \Rightarrow V_1 = V_2 \text{ (or } v_1 = v_2 \text{).}$$

- First Law: System

$$\Delta Q_2 = U_2 - U_1 + \Delta W_2^0 = m(u_2 - u_1)$$

$$\Delta Q_2 = 0.75 (1258.5355 - 2789.22)$$

$$= -1148.0 \text{ kJ}$$

(Negative sign indicates heat transfer from the system to surroundings) \Rightarrow Cooling process.

5.87

For an application the change in enthalpy of carbon dioxide from 30 to 1500°C at 100 kPa is needed. Consider the following methods and indicate the most accurate one.

- Constant specific heat, value from Table A.5.
- Constant specific heat, value at average temperature from the equation in Table A.6.
- Variable specific heat, integrating the equation in Table A.6.
- Enthalpy from ideal gas tables in Table A.8.

Solution:

$$\text{a) } \Delta h = C_{po}\Delta T = 0.842 (1500 - 30) = \mathbf{1237.7 \text{ kJ/kg}}$$

$$\text{b) } T_{ave} = \frac{1}{2} (30 + 1500) + 273.15 = 1038.15 \text{ K}; \quad \theta = T/1000 = 1.0382$$

$$\text{Table A.6} \Rightarrow C_{po} = 1.2513$$

$$\Delta h = C_{po,ave} \Delta T = 1.2513 \times 1470 = \mathbf{1839 \text{ kJ/kg}}$$

$$\text{c) } \text{For the entry to Table A.6: } \theta_2 = 1.77315; \quad \theta_1 = 0.30315$$

$$\Delta h = h_2 - h_1 = \int C_{po} dT$$

$$= [0.45 (\theta_2 - \theta_1) + 1.67 \times \frac{1}{2} (\theta_2^2 - \theta_1^2)$$

$$- 1.27 \times \frac{1}{3} (\theta_2^3 - \theta_1^3) + 0.39 \times \frac{1}{4} (\theta_2^4 - \theta_1^4)] = \mathbf{1762.76 \text{ kJ/kg}}$$

$$\text{d) } \Delta h = 1981.35 - 217.12 = \mathbf{1764.2 \text{ kJ/kg}}$$

The result in d) is best, very similar to c). For large ΔT or small ΔT at high T_{avg} , a) is very poor.

5.105

A piston/cylinder contains 0.001 m^3 air at 300 K , 150 kPa . The air is now compressed in a process in which $P V^{1.25} = C$ to a final pressure of 600 kPa . Find the work performed by the air and the heat transfer.

Solution:

C.V. Air. This is a control mass, values from Table A.5 are used.

$$\text{Continuity: } m_2 = m_1$$

$$\text{Energy Eq.5.11: } m(u_2 - u_1) = {}_1Q_2 - {}_1W_2$$

$$\text{Process: } P V^{1.25} = \text{const.}$$

$$\text{State 2: } V_2 = V_1 (P_1/P_2)^{1/1.25} = 0.00033 \text{ m}^3$$

$$T_2 = T_1 P_2 V_2 / (P_1 V_1) = 300 \frac{600 \times 0.00033}{150 \times 0.001} = 395.85 \text{ K}$$

$${}_1W_2 = \frac{1}{n-1} (P_2 V_2 - P_1 V_1) = \frac{1}{1.25-1} (600 \times 0.00033 - 150 \times 0.001) = -0.192 \text{ kJ}$$

$$\begin{aligned} {}_1Q_2 &= m(u_2 - u_1) + {}_1W_2 = \frac{P_1 V_1}{RT_1} C_v (T_2 - T_1) + {}_1W_2 \\ &= 0.001742 \times 0.717 \times 95.85 - 0.192 = -0.072 \text{ kJ} \end{aligned}$$